**Tishk International University Engineering Faculty Petroleum and Mining Engineering Department**



# **Petroleum Reservoir Engineering II**

**Lecture 6: Fundamentals of Reservoir Fluid Flow (III)**

**Third Grade- Spring Semester 2021-2022** 

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# Content:

- Derivation of Darcy's Law for steady-state:
- Linear Flow of Incompressible Fluids
- Linear Flow of Slightly Compressible Fluids
- Linear Flow of Compressible Fluids
- Radial Flow of Incompressible Fluids
- Radial Flow of Slightly Compressible Fluids
- Radial Flow of Compressible Fluids

• Linear Flow of Incompressible Fluids:

 $q =$ 

0.001127  $kA (p1-p2)$ 

 $\frac{1}{\mu}$  –  $\frac{1}{\mu}$  – (1)

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Where q= flow rate, bbl/day **Los** 

k= absolute permeability, md

p= pressure, psia

 $\mu$ = viscosity, cp

L= distance, ft

A= cross-sectional area,  $ft^2$ 

Radial Flow of Incompressible Fluids:

 $Q_o$ 

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 $-p_w$ )  $\mu_0 B_0 \ln(r_e/r_w)$ 

 $---(2)$ 

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Where  $Q_o$  = oil flow rate, STB/day

- $p_e$  = external pressure, psi
- $p_{wf}$  = bottom-hole flowing pressure, psi
- k= permeability, md
- $\mu_o$  = oil viscosity, cp
- $B<sub>o</sub>$  = oil formation volume factor, bbl/STB
- h = thickness, ft
- $r_e$  = external or drainage radius, ft
- $r_w$  = wellbore radius, ft

- Linear Flow of Slightly Compressible Fluids:
- The relationship that exists between pressure and volume for slightly compressible fluids has been discussed in the previous lecture and is described by following equation:

 $V = V_{ref}[1 + c(p_{ref} - p)]$ 

The above equation can be modified and written in terms of flow rate as:

 $= R$  =  $q_{ref}[1 + c(p_{ref} - p)]^{0.8}$  (3)

Where  $q_{ref}$  is the flow rate at some reference pressure  $p_{ref}$ .

• Linear Flow of Slightly Compressible Fluids:

 $q = q_{ref}[1 + c(p_{ref} - p)]$ 

Substituting the above relationship in Darcy's equation gives:

$$
\frac{q}{A} = \frac{q_{ref}[1 + c(p_{ref} - p)]}{A} = -0.001127 \frac{k}{\mu} \frac{dp}{dx}
$$

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■ Separating the variables and arranging:

$$
\frac{q_{ref}}{A} \int_{0}^{L} dx = -0.001127 \frac{k}{\mu} \int_{p_1}^{p_2} \left[ \frac{dp}{1 + c(p_{ref} - p)} \right]
$$

- Linear Flow of Slightly Compressible Fluids:
- Integrating gives:

$$
q_{ref} = \left[\frac{0.001127 \ kA}{\mu c} \right] \ln \left[\frac{1 + c(p_{ref} - p_2)}{1 + c(p_{ref} - p_1)}\right] \quad - \quad - (4)
$$

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Where  $q_{ref}$  = flow rate at a reference pressure  $p_{ref}$ , bbl/day

 $p_1$ = upstream pressure, psi

 $p_2$ = downstream pressure, psi

 $\mu$ = viscosity, cp

c= average liquid compressibility,  $psi^{-1}$ 

- Linear Flow of Slightly Compressible Fluids:
- **EXEDENT Selecting the upstream pressure**  $p_1$  **as the reference pressure**  $p_{ref}$  **and substituting in equation (4)** gives the flow rate at Point 1 as:

$$
q_1 = \left[\frac{0.001127 kA}{\mu cL}\right] ln[1 + c(p_1 - p_2)] \quad (5)
$$
\n
$$
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$$

- Linear Flow of Slightly Compressible Fluids:
- Choosing the downstream pressure  $p_2$  as the reference pressure and substituting in equation (4) gives:

$$
q_2 = \left[\frac{0.001127 \text{ kA}}{\mu cL}\right] \ln\left[\frac{1}{1 + c(p_2 - p_1)}\right] \quad - \quad - (6)
$$

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Where  $q_1$  and  $q_2$  are the flow rates at Points 1 and 2, respectively.

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• Linear Flow of Slightly Compressible Fluids:

Example 2: A slightly compressible liquid flows in a linear porous media with the following properties:



Calculate the flow rate at both ends of the linear system. The liquid has an average compressibility of 21  $*$  $10^{-5} psi^{-1}$ .

• Linear Flow of Slightly Compressible Fluids:

Solution:

• Choosing the upstream pressure as the reference pressure gives:

$$
q_1 = \left[\frac{(0.001127)(100)(6000)}{(2)(21*10^{-5})(2000)}\right] ln[1 + (21*10^{-5})(2000 - 1990)]
$$
  
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$$
q_1 = 1.689 \, bbl/day
$$

• Linear Flow of Slightly Compressible Fluids:

#### Solution:

Choosing the downstream pressure, gives:

$$
q_2 = \left[\frac{(0.001127)(100)(6000)}{(2)(21*10^{-5})(2000)}\right] ln \left[\frac{1}{1 + (21*10^{-5})(1990 - 2000)}\right]
$$
  
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The above calculations show that  $q_1$  and  $q_2$  are not largely different, which is due to the fact that the liquid is slightly compressible, and its volume is not a strong function of pressure.

- Linear Flow of Compressible Fluids:
- For a viscous (laminar) gas flow in a homogeneous-linear system, the real-gas equation of state can be applied to calculate the number of gas moles n at pressure p, temperature T, and volume V:

 $pV$ 

 $ZRT$ 

At standard conditions, the volume occupied by the above n moles is given by:

 $n=$ 

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$$
V_{sc} = \frac{n z_{sc} RT_{sc}}{p_{sc}} --- (8)
$$

- Linear Flow of Compressible Fluids:
- **Combining the above two expressions and assuming**  $z_{sc} = 1$  **gives:**

Equivalently, the above relation can be expressed in terms of the flow rate as: 2008

 $pV$ 

 $Z\overline{T}$ 

=

 $p_{sc}V_{sc}$ 

 $T_{sc}$ 

$$
\frac{5.615pq}{zT} = \frac{p_{sc}Q_{sc}}{T_{sc}}
$$

- Linear Flow of Compressible Fluids:
- Rearranging the previous equation:

$$
\left(\frac{p_{sc}}{T_{sc}}\right)\left(\frac{2T}{p}\right)\left(\frac{Q_{sc}}{5.615}\right) = q - \frac{9}{4}
$$

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Where  $q=$  gas flow rate at pressure p in bbl/day

 $Q_{sc}$  = gas flow rate at standard conditions, scf/day

z= gas compressibility factor

 $T_{sc}$ ,  $p_{sc}$  = standard temperature and pressure in  $\textdegree R$  and psia, respectively.

- Linear Flow of Compressible Fluids:
- Replacing the gas flow rate q with that Darcy's Law, i.e., equation (1) gives:

$$
\frac{q}{A} = \left(\frac{p_{sc}}{T_{sc}}\right) \left(\frac{zT}{p}\right) \left(\frac{Q_{sc}}{5.615}\right) \left(\frac{1}{A}\right) = -0.001127 \frac{k}{\mu} \frac{dp}{dx}
$$

- The constant 0.001127 is to convert from Darcy's units to field units.
- Separating variables and arranging yields:

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$$
\left[\frac{q_{sc}p_{sc}T}{0.006328 kT_{sc}A}\right]_0^L dx = -\int_{p_1}^{p_2} \frac{p}{z\mu_g} dp
$$

- Linear Flow of Compressible Fluids:
- Assuming constant z and  $\mu_g$  over the specified pressure, i.e.,  $p_1$  and  $p_2$ , and integrating gives:

0.003164 $T_{sc}A k (p_1^2 - p_2^2)$ 

 $p_{sc}TLz\mu_g$ 

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 $Q_{sc}$  =

Where  $Q_{sc}$  = gas flow rate at standard conditions, scf/day

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- k= permeability, md
- T= temperature, °R
- $\mu_g$  = gas viscosity, cp
- A= cross-sectional area,  $ft^2$

L= total length of the linear system, ft

- Linear Flow of Compressible Fluids:
- Setting  $p_{sc}$  = 14.7 psi and  $T_{sc}$  = 520 °R in the above expression gives:

 $Q_{sc}$  = 0.111924Ak  $(p_1^2-p_2^2)$  $TLz\mu_g$  $(10)$ 

The above equation is valid for applications when the pressure<2,000 psi. The gas properties must be evaluated at the average pressure  $\bar{p}$  as defined below:

$$
\bar{p} = \sqrt{\frac{p_1^2 + p_2^2}{2}} \, \text{---} \, \text{---} \, (11)
$$

Linear Flow of Compressible Fluids:

Example: A linear porous media is flowing a 0.72 specific gravity gas at 120°F. The upstream and downstream pressures are 2,100 psi and 1,894.73 psi, respectively. The cross-sectional area is constant at  $4,500\, ft^2$ . The total length is 2,500 feet with an absolute permeability of 60md. Calculate the gas flow rate in scf/day ( $p_{sc} = 14.7$  psia,  $T_{sc} = 520 \degree R$ ).

- Radial Flow of Slightly Compressible Fluids:
- The relation of pressure and flow rate has been determined previously by following equation:

 $q = q_{ref}[1 + c(p_{ref} - p)]$ 

If above equation is substituted into the radial form of Darcy's Law:

$$
\mathsf{ERB}_v = \frac{q}{A_r} = \frac{q}{2\pi rh} = 0.001127 \frac{k \, dp}{\mu \, dr}
$$

The following is obtained:

$$
\frac{q}{A_r} = \frac{q_{ref}[1 + c(p_{ref} - p)]}{2\pi rh} = 0.001127 \frac{k}{\mu} \frac{dp}{dr}
$$

Where  $q_{ref}$  is the flow rate at some reference pressure  $p_{ref}$ .

Or

- Radial Flow of Slightly Compressible Fluids:
- Separating the variables in the above equation and integrating over the length of the porous medium gives:

$$
\frac{q_{ref}\mu}{2\pi kh} \int_{rw}^{r_e} \frac{dr}{r} = 0.001127 \int_{p_{wf}}^{p_e} \frac{dp}{1 + c(p_{ref} - p)}
$$
\n
$$
q_{ref} = \left[\frac{0.00708 \, kh}{\mu \, c \ln\left(\frac{r_e}{r_w}\right)}\right] \ln\left[\frac{1 + c(p_e - p_{ref})}{1 + c(p_{wf} - p_{ref})}\right]
$$

Where  $q_{ref}$  is oil flow rate at a reference pressure  $p_{ref}$ .

- Radial Flow of Slightly Compressible Fluids:
- Choosing the bottom-hole flow pressure  $p_{wf}$  as the reference pressure and expressing the

flow rate in STB/day gives:

$$
Q_o = \left[\frac{0.00708 \, kh}{\mu_o B_o c_o \, ln\left(\frac{r_e}{r_w}\right)}\right] \ln\left[1 + c_o (p_e - p_{wf})\right] - -(5)
$$

Where  $c_0$ = isothermal compressibility coefficient,  $psi^{-1}$ 

 $Q<sub>o</sub>$  = oil flow rate, STB/day

k= permeability, md

• Radial Flow of Slightly Compressible Fluids:

Example: The following data are available on a well in the Red River Field:

 $p_e$  = 2506 psi  $p_{wf}$  = 1800  $r_e$  = 745′  $r_w$  = 0.25  $B_0 = 1.25$   $\mu_0 = 2.5$   $c = 25 * 10^{-6} \text{psi}^{-1}$ k= 0.12 Darcy h= 25 ft.

Assuming a slightly compressible fluid, calculate the oil flow rate. Compare the result with that of incompressible fluid.

• Radial Flow of Slightly Compressible Fluids:

Solution:

For a slightly compressible fluid, the oil flow rate can be calculated by applying equation (5):

$$
Q_o = \left[ \frac{(0.00708)(120)(25)}{(2.5)(1.25)(25*10^{-6})\ln(745/0.25)} \right] * \ln[1 + (25*10^{-6})(2506 - 1800)]
$$
  
\n
$$
Q_o = 595 STB/day
$$

• Radial Flow of Slightly Compressible Fluids:

Solution:

Assuming an incompressible fluid, the flow rate can be estimated by applying Darcy's equation,

i.e., equation (2):

 $Q_o =$  $(0.00708)(120)(25)(2506 - 1800)$  $2.5$  $(1.25)$  $ln(745/0.25)$ 

 $Q_o = 600 \, STB/day$ 

- Radial Flow of Compressible Fluids:
- The basic differential form of Darcy's Law for a horizontal laminar flow is valid for describing the flow of both gas and liquid systems.

 $\sim$ 

For a radial gas flow, the Darcy's equation takes the form:



- Radial Flow of Compressible Fluids:
- The gas flow rate is usually expressed in scf/day. Referring to the gas flow rate at standard condition as  $Q_g$ , the gas flow rate  $q_{gr}$  under pressure and temperature can be converted to that of standard condition by applying the real gas equation-of-state to both conditions, or:

$$
\text{ERBIL} \quad \frac{5.615 \, q_{gr} \, p}{zTR} = \frac{Q_g \, p_{sc}}{z_{sc} R \, T_{sc}}
$$
\n
$$
\left(\frac{p_{sc}}{5.615 \, T_{sc}}\right) \left(\frac{zT}{p}\right) Q_g = q_{gr} \, --- (7)
$$

Or

• Radial Flow of Compressible Fluids:

 $p_{sc}$ 5.615  $Z\overline{T}$  $\overline{p}$  $q_{ar}$ 

 $\sim$ 

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Where  $p_{sc}$  = standard pressure, psia

- $T_{sc}$  = standard temperature,  ${}^{\circ}R$
- $Q_q$  = gas flow rate, scf/day
- $q_{ar}$  = gas flow rate at radius r, bbl/day
- p= pressure at radius r, psia
- T= reservoir temperature, °R
- z= gas compressibility factor at p and T

 $z_{sc}$  = gas compressibility factor at standard condition  $\approx 1.0$ 

 $\leftarrow$ 

- Radial Flow of Compressible Fluids:
- Combining equations (6) and (7) yields:

$$
\left(\frac{p_{sc}}{5.615 T_{sc}}\right) \left(\frac{\text{zT}}{\text{p}}\right) Q_g = \frac{0.001127(2\pi rh)k}{\mu_g} \frac{dp}{dr}
$$

**E** Assuming that  $T_{sc}$  = 520 °R and  $p_{sc}$  = 14.7 psia:

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$$
\left(\frac{TQ_g}{k h}\right)\frac{dr}{r} = 0.703 \left(\frac{2p}{\mu_g z}\right)dp - -(8)
$$

- Radial Flow of Compressible Fluids:
- **Integrating equation (8) form the wellbore conditions**  $(r_w$  **and**  $p_{wf}$ **) to any point in the** reservoir (r and p) gives:

$$
\int_{r_w}^{r} \left(\frac{T Q_g}{k h}\right) \frac{dr}{r} = 0.703 \int_{p_{wf}}^{p} \left(\frac{2p}{\mu_g z}\right) dp
$$
 (9)

- Radial Flow of Compressible Fluids:
- Imposing Darcy's Law conditions on equation (9), i.e.:
- Steady-state flow, which requires that  $Q_q$  is constant at all radii

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Homogeneous formation, which implies that k and h are constant

gives:

 $TQ_g$  $k h$ ln  $\boldsymbol{r}$  $r_{\!\scriptscriptstyle (\!\chi\!)}$  $= 0.703$  $p_{wf}$  $\overline{p}$  $2p$  $\mu_g$ z  $\,dp$ 

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- Radial Flow of Compressible Fluids:
- **•** The term  $\int_{p_{wf}}^{p} \left( \frac{2p}{\mu_{g}^2} \right)$  $\mu_g$ z  $dp$  can be expanded to give:

$$
\int_{p_{wf}}^{p} \left(\frac{2p}{\mu_g z}\right) dp = \int_{0}^{p} \left(\frac{2p}{\mu_g z}\right) dp - \int_{0}^{p_{wf}} \left(\frac{2p}{\mu_g z}\right) dp
$$

■ Combining the above relationships yields:

$$
\left(\frac{TQ_g}{k h}\right) \ln\left(\frac{r}{r_w}\right) = 0.703 \left[ \int\limits_0^p \left(\frac{2p}{\mu_g z}\right) dp - \int\limits_0^{p_W f} \left(\frac{2p}{\mu_g z}\right) dp \right] - -(10)
$$

- Radial Flow of Compressible Fluids:
- **•** The integral  $\int_0^p \left(\frac{2p}{\mu_a^2}\right)$  $\mu_g$ z  $dp$  is called the real gas potential or real gas pseudopressure, and it is usually represented by  $m(p)$  or  $\psi$ . Thus

$$
m(p) = \psi = \int\limits_{0}^{p} \left(\frac{2p}{\mu_{g}z}\right) dp
$$
---(11)

Equation (10) can be written in terms of the real gas potential to give:

$$
\left(\frac{TQ_g}{k h}\right) \ln \left(\frac{r}{r_w}\right) = 0.703(\psi - \psi_w)
$$

Or 
$$
\psi = \psi_w + \frac{Q_g T}{0.703 \, kh} \ln \frac{r}{r_w} - \frac{-(12)}{}
$$

- Radial Flow of Compressible Fluids:
- Equation (12) indicates that a graph of  $\psi$ vs.  $ln r/r_w$  yields a straight line of slope  $(Q_q T/0.703 kh)$  and intercept  $\psi_w$  as **ERBIL** shown in the figure:



- Radial Flow of Compressible Fluids:
- The flow rate is given exactly by:

$$
Q_g = \frac{0.703 \; kh(\psi - \psi_w)}{T \; ln \frac{r}{r_w}} \qquad (13)
$$

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In the particular case when  $r = r_e$ , then:

$$
Q_g = \frac{0.703 \, kh(\psi_e - \psi_w)}{T \, ln \frac{r_e}{r_w}} \, --- (14)
$$

- Radial Flow of Compressible Fluids:
- The gas flow rate is commonly expressed in Mscf/day, or:

$$
Q_g = \frac{kh(\psi_e - \psi_w)}{1422T \ln \frac{r_e}{r_w}} \quad - \quad - (15)
$$

Where  $Q_g$ = gas flow rate, Mscf/day

 $\psi_{e}$ = real gas potential <mark>as e</mark>valuated from 0 to  $p_{e}$ ,  $psi^{2}/cp$ 2008

 $\psi_w$ = real gas potential as evaluated from 0 to  $p_{wf}$ ,  $psi^2/cp$ 

k= permeability, md

h= thickness, ft

 $r_e$  = drainage radius, ft

 $r_w$  = wellbore radius, ft